Availability of Mercury Control Technology

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What do we know about controlling mercury?

- Solutions come in different shapes and sizes
- Already tremendous progress and investments
- Regulations create market certainty ... driving R&D and commercial competition for lower cost solutions
- Most mercury control is about finding new and improved uses for existing technologies and then some.

Wide Range of Control Options

Co-benefits

- SCR, FGD, ESP, FF, etc.

Enhanced co-benefits

- Chemical oxidants
- Adding additional catalyst layers or new oxidizing catalyst
- Non-carbon based sorbents
- Chemically-Enhanced sorbents
- High energy excitation

Combustion modifications

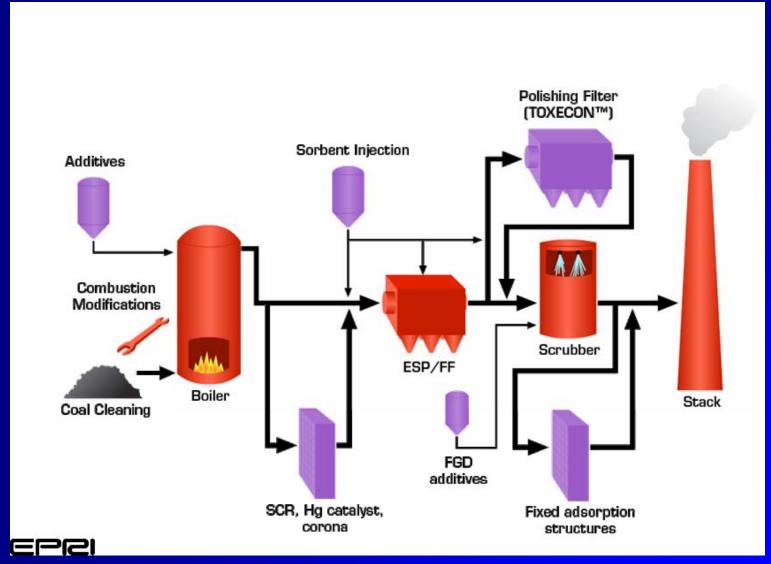
- In boiler modifications to oxidize mercury and increase amount of carbon (i.e. research and demos at Lehigh University and GE Energy)
- State-of-the-Science Ultra-Super Critical Boilers with advanced APC

Precombustion

- K-fuel: cost in scrubbing coal; can be combined with other controls
- Gasification: up front equipment cost to convert from solid to gaseous fuel; requires pollutant disposal

Sorbents (ACI/PAC)

Power Plant Mercury Control Options



Some Bituminous Coal Control Strategies

Bituminous coals typically have moderate-high Cl/Br content and higher sulfur levels:

"the right stuff" for mercury and SO₂ control

Configuration

No FGD: ACI/PAC, and add fabric filter option if:

- desire higher mercury removal efficiency, and/or
- ash sale

<u>Dry FGD</u>: ACI/PAC (may already have fabric filter)

Wet FGD: improve and control mercury oxidation

Co-Benefits/Multipollutant Approach – timing and labor

Wet FGD:

- 19 to 30 months to construct (avg. in mid-20's); 180 man-years
- Components: grinding mill, slurry prep., reactor vessel, dewatering and gypsum stacking

• SCR:

- 13 to 24 months to construct (avg. in low 20's); 170 man-years
- Components: structural steel, NH₃ injection grid, catalyst reactor bed, catalyst, by-pass duct (?)
- * Need for early planning decisions

Recent Wet FGD Co-Benefit ... Plus

Mount Storm Site Test (WV)

- Eastern Bituminous Coal
 - medium sulfur (1.82%)
 - 4,000 tons/day
- 1662 MW (3 units combined)
- Air Pollution Controls
 - SCR 2 layers
 - ESP
 - wet FGD forced oxidation limestone

Results of Co-Benefit ... Plus

70% mercury removal with only wet FGD

some mercury re-emission at outlet

80% mercury removal with wet FGD plus additive (w/o SCR)

- additive stopped mercury re-emission
- SO₂ removal by wet FGD system not impacted by additive technology

90% plus mercury removal with wet FGD & SCR

- > 95% of mercury in oxidized state after SCR
- similar results with/without FGD additive (no mercury re-emission to control)
- Demonstrated improvements using wet FGD additive process (B&W patented sodium hydrosulfide)
 - Improved removal of mercury w/o SCR in-service
 - Cost-effective incremental mercury removal (w/o activated carbon injection)

Additional Multipollutant Control Options

Powerspan ECO Process

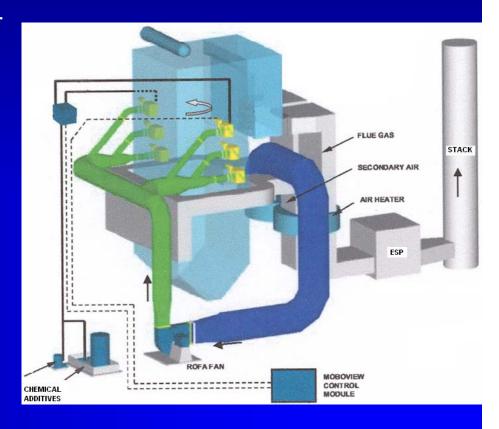
- Integrated Control Approach
- High Energy Corona
- First Energy Pilot Plant
 - Burger Plant 50 MW size
 - 98% SO₂
 - $-90\% NO_{x}$
 - 80-90% Hg
 - 95% PM_{2.5}
- Commercial Application
 - FirstEnergy 215 MW Bay Shore Plant Unit 4
 - Operational 1st Quarter 2006
 - Costs \$100 million
 - Creates Saleable Fertilizer Byproduct



Additional Multipollutant Control Options (cont.)

Mobotec Rofa & Rotamix Technologies

- MINPlus Sorbent Injection in Boiler
- Scrubber After Boiler
- Performance
 - $-60 \% NO_{x}$
 - 65 % SO₂
 - Up to 90 % Hg
- Commercial Application
 - Minnesota Power
 - Taconite Harbor Energy Center
 - Startup 2006-2008 timeframe
 - \$60 million (includes NO_x control for Laskin Unit too)



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Precombustion Control Option

KFx K-Fuel Process

- Coal Cleaning
- High Temp. and Pressure
- Western Low Btu Coals

Benefits

- Increases BTU by 30-40%
- Removes Pollutants
 - 70% Hg
 - 30 % SO₂ and NO_x
 - Potential Tax Incentives

Production Facilities

- Gillette, WY 750,000 tpy (2005)
- Buckskin Mine, WY 4 MMtpy (2008)
- Coal Creek Mine, WY 8 MMtpy (2008)
- Supply Approximately 3000 MW of Coal-Fired Plant Capacity



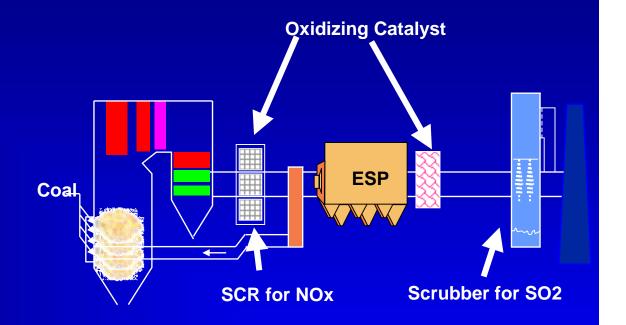
Postcombustion Control Option - Catalytic Oxidation

Catalytic Oxidation

- Converts Hg⁰ to Hg²⁺
- Hg²⁺ Water Soluble
- Configurations
 - Catalyst in SCR
 - Catalyst before Scrubber
 - Multiple Vendors &

Configurations

- Application & Performance
 - Oxidized Mercury (Hg²⁺) Captured in Scrubber
 - Applied to Coals w/ High Elemental Mercury (Hg⁰)
 - 5 to 50 % Additional Capture Hg



General Improvements for Mercury Control

- Techniques to enhance and control mercury oxidation
- Techniques to minimize re-emission
- Potential impacts on by-products
- Less capital intensive techniques
- Cost of mercury removal is coming down

Continuous Emissions Monitoring

- Continuous Hg measurements are being made today
 - At least 6 suppliers of instruments
 - Current instruments are highly accurate* but high-maintenance
 - Technology rapidly advancing toward increased reliability and less frequent maintenance so it could be operated by plant personnel
- Compliance and/or real-time control information

^{*} CEMS that have passed RATA are at least as accurate as the reference method

Summary of Other State Rules and Programs

Connecticut

- 2003 state legislation
- 2 facilities affected
- 0.6 lb/TBtu or 90% by July 2008; 2012 review of all sources
- "soft landing flexibility" if done properly and can't meet limit, consider for alternate limit
- CEMS if available

New Jersey

- 2004 rule adoption of broad industry mercury control (7 bit. coal-fired, iron & steel, MSW & med. Incinerators)
- By 12/15 2007 achieve 90% or rate of 3.0 mg/MW-hr on annual rolling avg. weighted by MW output
- Flexibility: if enforceable multi-pollutant agreement, then 12/15 2012; potential plant averaging
- Quarterly stack testing; CEMS if federal performance specification and technology available

Summary of Other State Rules and Programs (cont.)

Massachusetts

- 2004 adoption of final caps (multi-pollutant)
- 4 facilities affected; bituminous
- 2 Phase Program
 - Phase 1: By 2006-2008 achieve 85% or 0.0075 lb/net GW-hr of electricity generated (annual rolling avg.)
 - Phase II: By 10/1 2012 achieve 95% or 0.0025 lb/net GW-hr
- Flexibility: early reductions, off-site reductions, plant averaging
- CEMS by 2008

Wisconsin

- 2004 regulation requires adoption of federal rule
- 4 utilities with 42 units (>25 MW) affected; bituminous/subbituminous
- 2 Phases: 45% reduction by 2010; 75% by 2015
- 80% by 2018 (to encourage additional progress)
- New & modified units capped at 10 lb/yr
- Flexibility: variance requests based on costs or technology availability; early reduction banking starting 10/1 2004; remain at Hg baseline if opt for 2 of 4 pollutant reduction requirements

Other States: legislation, consideration

Delaware

Indiana

Michigan

Montana

Illinois

New Hampshire

Minnesota

North Carolina

Iowa (permit)

STAPPA/ALAPCO Model Rule

- Released Nov 14, 2005
- Flexibilities:
 - Annual rolling averages
 - Averaging/bubble emissions across facility
 - Two phases
 - 2nd Phase option is multipollutant commitment
 - Promotes facilities continued power generation
 - Slower than MACT; much further & faster than CAMR
 - Coal neutral

Keys to Cost-Effective Multi-Pollutant Controls: APC Industry Perspective

- Clear timetable and requirements to control all pollutants
 - Multi-pollutant control approach, if aggressive, could simultaneously address mercury, PM_{2.5}, regional haze, ozone transport, and 8-hour ozone standard, thus lowering the evaluated cost for each regulatory program
 - Allows development of integrated compliance plans utilizing existing equipment
 - Clarity, enforcement, & flexibility for well-defined unusual sitespecific conditions
- Performance-based Rules
 - Maximize incentives for innovation and competition
 - Life is too unpredictable -- e.g., fuel costs, technology innovation -for government to pick technology winners and losers

For More:

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